

5 Juri M. Seletzky · Ute Noack · Jens Fricke ·
6 Sebastian Hahn · Jochen Büchs

7 **Metabolic activity of *Corynebacterium glutamicum* grown**
8 **on L-lactic acid under stress**

9 Received: 17 January 2006 / Revised: 19 March 2006 / Accepted: 23 March 2006
10 © Springer-Verlag 2006

11 **Abstract** Respiration measurement in shake flasks is in-
12 troduced as a new method to characterize the metabolic
13 activity of microorganisms during and after stress expo-
14 sure. The major advantage of the new method is the pos-
15 sibility to determine the metabolic activity independent
16 of manual sampling without the necessity to change the
17 culture vessel or the cultivation medium. This excludes
18 stress factors, which may be induced by transferring the
19 microorganisms to plates or respirometers. The negative
20 influence interruptions of the shaker during sampling times
21 which may have on the growth of microorganisms was
22 demonstrated. The applicability of the method was ver-
23 ified by characterizing the behavior of *Corynebacterium*
24 *glutamicum* grown on the carbon source L-lactic acid under
25 the stress factors such as carbon starvation, anaerobic
26 conditions, lactic acid, osmolarity, and pH. The following
27 conditions had no effect on the metabolic activity of
28 *C. glutamicum*: a carbon starvation of up to 19 h, anaerobic
29 conditions, lactic acid concentrations up to 10 g/l, 3-
30 (*N*-morpholino)propanesulfonic acid buffer concentrations
31 up to 42 g/l, or pH from 6.4 to 7.4. Lactic-acid concen-
32 trations from 10 to 30 g/l lead to a decrease of the growth
33 rate and the biomass substrate yield without effecting
34 the oxygen substrate conversion. Without adaptation, the
35 organism did not grow at $\text{pH} \leq 5$ or ≥ 9 .

36 **Introduction**

37 Stress tolerance and stress adaptation of microorganisms
38 has been characterized to understand the survival strategies
39 of pathogenic organisms like *Mycobacterium tuberculosis*
40 (Hu and Coates 1999; Primm et al. 2000) and *Staphylo-*
41 *coccus aureus* (Watson et al. 1998), or food-spoiling

bacteria like *Listeria monocytogenes* (Ferreira et al. 2001) 42
and *Listeria innocua* (Houtsma et al. 1996). *Escherichia* 43
coli was used by several researchers (Breidt et al. 2004; 44
Ihssen and Egli 2004; Mandel and Silhavy 2005; Presser 45
et al. 1997, 1998; Roe et al. 2002; Ross et al. 2003) to study 46
the stress tolerance and stress response of Gram-negative 47
organisms. Microorganisms have developed complex stress- 48
survival and stress-response strategies to respond to various 49
stress factors like starvation, oxygen, osmolarity, or pH. 50
The knowledge about these strategies has increased funda- 51
mentally in the last decade due to the advances of 52
molecular biological methods. However, the standard 53
methods to determine the viability and activity after and 54
during stress have remained unchanged. Viable cell counts 55
with petri dishes and activity determination with respirom- 56
etry are still the most common methods to determine the 57
interaction between microorganisms and stress. 58

In this study, a new method is introduced to continuously 59
monitor the oxygen transfer rate (OTR) of microorganisms 60
in shake flasks during and after exposure to stress without 61
the necessity to change the culture vessel or the medium. 62
The OTR reflects the metabolic activity and in most cases 63
also the growth rate of microorganisms due to the fact 64
that almost every physiological activity in aerobic cultures 65
is coupled to the respiratory uptake of oxygen (Anderlei 66
et al. 2004; Anderlei and Büchs 2000; Losen et al. 2004; 67
Stöckmann et al. 2003). The new method has three major 68
advantages over the standard methods: (1) Cultivation and 69
metabolic activity determination are performed in the same 70
culture vessel and in the same medium, excluding stress 71
factors which may be induced by transferring the micro- 72
organisms to plates or respirometers. (2) Continuous online 73
monitoring enables the determination of the metabolic 74
activity independent of the sampling interval. (3) The 75
sampling times for molecular stress-response analysis 76
can be chosen in a flexible way according to the online- 77
monitored behavior of the culture and not according to a 78
fixed, predetermined sampling schedule. The mentioned 79
advantages are all part of the technical nature of the 80
measuring technique. How important they are can only be 81
determined through a direct comparison with alternative 82

J. M. Seletzky · U. Noack · J. Fricke · S. Hahn · J. Büchs (✉)
Biochemical Engineering, RWTH Aachen University,
Sammelbau Biologie, Worringerweg 1,
52056 Aachen, Germany
e-mail: buechs@biovt.rwth-aachen.de
Tel.: +49-241-8025546
Fax: +49-241-8022265

83 methods, which was not the focus of this study. The broad
84 applicability of the method is demonstrated by analyzing
85 the behavior of *Corynebacterium glutamicum* on minimal
86 medium with L-lactic acid as sole carbon source under the
87 stress factors such as carbon starvation, anaerobic condi-
88 tions, lactic acid, osmolarity, and pH.

89 The physiological behavior of biological cultures can be
90 derived from the OTR by analyzing the slope and the form
91 of the OTR curve (Anderlei et al. 2004; Anderlei and
92 Büchs 2000; Losen et al. 2004; Stöckmann et al. 2003); in
93 addition, the integral of the OTR curve can be used to
94 control the stoichiometry and the exhaustion of essential
95 nutrients (Stöckmann et al. 2003). In the very most cases,
96 the OTR can be used as sole measuring parameter to study
97 the stress response of microorganisms growing on any
98 carbon source, if not oxygen-limited conditions are of
99 interest. Oxygen-limited (not anaerobic) conditions can be
100 investigated by considering the OTR and the carbon
101 dioxide transfer rate (Anderlei et al. 2004) if the anaerobic
102 product is consumed by diauxic growth and/or the carbon
103 source and its anaerobic product have a different degree of
104 reduction (e.g., glucose and ethanol). Different from most
105 organisms, *C. glutamicum* does not show diauxic growth
106 but coutilization if grown on mixtures of carbon sources
107 glucose/lactate (Cocaign et al. 1993) or glucose/acetate
108 (Wendisch et al. 2000). The applicability of the new tech-
109 nology to study oxygen-limited *C. glutamicum* glucose
110 cultures is further hampered by the fact that glucose and
111 its anaerobic product lactate have the same degree of
112 reduction. *C. glutamicum* grown on lactic acid as carbon
113 source does not produce an anaerobic product under
114 oxygen-limited conditions. Thus, the stress response of
115 *C. glutamicum* can be investigated under oxygen-unlimited
116 and oxygen-limited conditions if the carbon source lactic
117 acid is used. Instead of using lactic acid, it would have been
118 possible to use glucose and limit the study to oxygen-
119 unlimited conditions.

120 *C. glutamicum* is widely used for the industrial pro-
121 duction of amino acids. It is a high-G+C Gram-positive soil
122 bacterium and closely related to the Brevibacteria and
123 Mycobacteria (Gruber and Bryant 1997; Kinoshita et al.
124 1957). Stress behavior and amino acid production are
125 linked because external triggers like biotin limitation or
126 heat stress are often required to start amino acid production
127 (Barreiro et al. 2004, 2005; Gutmann et al. 1992; Stansen
128 et al. 2005). To improve amino acid production, the re-
129 sponse of *C. glutamicum* to substrate limitations/star-
130 vations has been intensively investigated with a strong
131 focus on nitrogen (Burkovski 2003; Nolden et al. 2001;
132 Silberbach et al. 2005) and phosphate (Ishige et al. 2003;
133 Kočan et al. 2006). Further interest in the stress response
134 of *C. glutamicum* comes from medical research. *C.*
135 *glutamicum* as a nonhazardous organism is considered an
136 ideal model to understand the stress response of closely
137 related pathogenic species, such as *Corynebacterium*
138 *diphtheriae*, *Mycobacterium leprae*, and *M. tuberculosis*.
139 Physiological observations of *C. glutamicum* on lactate
140 under standard batch and continuous conditions have been
141 reported by Cocaign et al. (1993), Cocaign-Bousquet and

Lindley (1995), and Gourdon et al. (2000). Studies of
L- and D-lactate metabolism and gene expression have been
mainly aimed at lactate dehydrogenase, anaplerotic reac-
tions, coutilization of lactate and other carbon sources, and
pyruvate accumulation (Cocaign et al. 1993; Gourdon et al.
2000; Koffas et al. 2003; Stansen et al. 2005).

Materials and methods

Microorganism, media, and culture conditions

Experiments were carried out with the wild type of
C. glutamicum ATCC 13032 (Kinoshita et al. 1957).
Complex medium liquid precultures were inoculated from
a complex medium plate culture. The complex medium
contained per liter: 20 g glucose, 10 g yeast extract, 10 g
peptone, 2.5 g NaCl, and 0.25 g MgSO₄. The pH was
adjusted to 7.2 and the glucose was sterilized separately.
The precultures reached a final pH of ~7.4.

The precultures were harvested after 12 h and washed
twice in 9 g/l NaCl. The pellet was resuspended in minimal
medium, and the minimal medium main culture was
inoculated with a biomass concentration of 0.25 g/l. The
temperature for all cultivations was 30 °C.

The minimal medium contained per liter: between 1 and
29.5 g lactic acid as specified in the results part, 20 g
(NH₄)₂SO₄, 1 g KH₂PO₄, 2 g K₂HPO₄, 0.25 g MgSO₄·
7H₂O, 30 mg 3,4-dihydroxybenzoic acid [(HO)₂C₆H₃
COOH], 10 mg CaCl₂·H₂O, 10 mg MnSO₄·H₂O, 10 mg
FeSO₄·7H₂O, 1 mg ZnSO₄·7H₂O, 0.2 mg CuSO₄, 0.2 mg
biotin, and 0.02 mg NiCl₂·7H₂O. For one experiment, 42 g
(0.2 M) 3-(N-morpholino)propanesulfonic acid (MOPS)
buffer was added. The initial pH was adjusted with NaOH
between 4 and 9.5, as specified in the results part. Trace
elements, biotin, 3,4-dihydroxybenzoic acid, and lactic
acid were sterilized separately. The lactic acid (80 % Karl
Roth GmbH, Karlsruhe, Germany) contained =950 g/l
L(+)-lactic acid. Cultures were cultivated on an orbital
shaker (Lab-Shaker LS-W, Adolf Kühner AG, Birsfelden,
Switzerland) with a filling volume of 10 (oxygen-un-
limited), 25, 30, or 60 ml (oxygen-limited conditions),
with a 50-mm shaking diameter and a 300-rpm shaking
frequency. Cultivations were carried out in unbaffled
250 ml Erlenmeyer flasks with cotton plugs or in 250 ml
measuring flasks of the RAMOS device (Anderlei et al.
2004; Anderlei and Büchs 2000). The maximum oxygen
transfer capacity (OTR_{max}) of the different culture condi-
tions was estimated according to the shake flask model of
Maier and Büchs (2001) and Maier et al. (2004). A single
inoculated medium was prepared for each experiment. This
inoculated medium was then distributed to each shake
flask. Only the flasks with different initial lactic acid
concentrations and the flasks with MOPS buffer were
inoculated separately. None of the experiments required a
change of measuring device, measuring vessel, or the
medium during the experiment, thus, avoiding metabolic
activity losses produced by transferring the microorgan-
isms to, e.g., respirometers or plates.

197	The final biomass concentration was determined by	253
198	centrifuging 1.5 ml of culture broth at 14,000 rpm in a dried	254
199	(24 h, 105 °C, cooled down in a dessicator) and weighed	255
200	microcentrifuge tube. After removing the supernatant, the	256
201	pellet was dried (24 h, 105 °C, cooled down in a dessicator)	257
202	and weighed. The biomass concentration of samples taken	258
203	during the experiment was calculated using an optical	259
204	density (OD ₆₀₀) dry weight correlation.	260
205	Titration curves were recorded by stepwise, adding	261
206	0.5 M NaOH to the medium, but never increasing the pH	262
207	by more than 0.1. Titration curves were recorded for three	
208	different media: the standard medium at the time of	
209	inoculation with 10 g/l lactic acid and 20 g/l (NH ₄) ₂ SO ₄ , a	
210	medium without lactic acid but with 20 g/l (NH ₄) ₂ SO ₄	
211	reflecting the conditions after the consumption of the	
212	carbon source, and a medium with 10 g/l lactic acid but	
213	without (NH ₄) ₂ SO ₄ . To increase the comparability, the	
214	titration curves were normalized to pH 7, which is the	
215	initial pH of the biological cultures. The normalization was	
216	done by subtracting the volume of 0.5 M NaOH necessary	
217	to adjust the pH to 7 from the actual titration volume giving	
218	positive volumes for pH greater than 7 and negative	
219	volumes for pH smaller than 7.	
220	The OTR was measured with a RAMOS device (Hitec	
221	Zang, Herzogenrath, Germany). The OTR is measured by	
222	periodically repeating an automated measuring cycle. A	
223	measuring cycle is composed of a measuring phase (flask	
224	closed air-tight, 10 min) and a rinsing phase (flushed air,	
225	20 min). The OTR is calculated from the decrease of the	
226	partial oxygen pressure in the headspace of the shake flask	
227	during the measuring phase. The rinsing phase can be	
228	operated in the one-flow or in the two-flow mode. The two-	
229	flow mode consists of a high aeration at the beginning of	
230	the rinsing phase and a low aeration for the rest of the	
231	rinsing phase. It recreates the average oxygen supply of a	
232	standard flask with a cotton plug (Anderlei et al. 2004). The	
233	variation of the partial oxygen pressure in the headspace of	
234	the shake flask caused by the measuring cycle is smaller	
235	than the differences in partial oxygen pressure produced by	
236	the variability of manually produced cotton plugs (Anderlei	
237	et al. 2004; Mrotzek et al. 2001). Thus, the stresses im-	
238	posed by standard flasks and RAMOS device are compar-	
239	able. The one-flow mode allows an increase of OTR _{max}	
240	in comparison to a standard flask with a cotton plug by	
241	aerating the entire rinsing phase with the high aeration.	
242	If during the cultivation the shaker had to be stopped,	
243	e.g., to take samples, the necessary manipulation time was	
244	recorded. The manipulation time includes the sampling	
245	time for all eight RAMOS flasks or ten standard flasks	
246	and the time which the shaker needs to decelerate and re-	
247	accelerate to the set shaking frequency.	
248	Stress induced by carbon starvation	
249	To investigate the influence of carbon starvation on the	
250	metabolic activity of <i>C. glutamicum</i> , the microorganisms	
251	were grown in batch fermentations with 10 g/l lactic acid	
252	and then starved. The metabolic activity was tested by	
	adding a lactic acid pulse after 28 h. After the pulse, the	253
	medium contained 5 g/l lactic acid. At the time of the pulse,	254
	the OTR of all cultures was below 0.001 mol/l/h. The pulse	255
	was added to the cultures during the rinsing phase of the	256
	RAMOS device 10 min before the start of the next mea-	257
	suring phase. Oxygen-unlimited and oxygen-limited cul-	258
	ture conditions were set by using filling volumes of 10, 30,	259
	and 60 ml. The initial pH was 7. The only manipulation	260
	necessary during the experiment was to stop the shaker for	261
	~10 min to add the lactic acid pulse.	262
	Stress induced by anaerobic conditions	263
	The behavior of <i>C. glutamicum</i> on lactic acid under an-	264
	aerobic conditions was investigated by comparing stan-	265
	dard batch cultures (aerated with air) with batch cultures	266
	aerated twice for 1 h with nitrogen. After starting the	267
	nitrogen aeration, it was verified with the oxygen sensor	268
	of the RAMOS device that the oxygen concentration in	269
	the flasks reached zero in less than 5 min. The anaerobic	270
	conditions were terminated by flushing the flasks with	271
	compressed air. Standard oxygen concentrations were	272
	reached again in less than 5 min. The nitrogen aeration	273
	was connected to the flask during the rinsing phase	274
	10 min before the start of the next measuring phase and	275
	disconnected directly after the previous measuring phase.	276
	Oxygen-unlimited and oxygen-limited (not anaerobic)	277
	culture conditions were set by using filling volumes of	278
	10, 30, and 60 ml. The lactic acid concentration was 10 g/l	279
	and the initial pH was 7. The only manipulation necessary	280
	during the experiment was stopping the shaker for ~5 min	281
	to connect and disconnect the nitrogen aeration.	282
	The influence of a delayed agitation and aeration after	283
	inoculation on the growth of <i>C. glutamicum</i> was inves-	284
	tigated by comparing cultures, which were directly shaken	285
	after inoculation with cultures which were not shaken after	286
	inoculation for 1, 2, and 3 h. To assure equal culture	287
	conditions of shaken and unshaken cultures, the unshaken	288
	flasks were placed directly next to the shaker in the same	289
	thermo-constant room. The filling volume was 25 ml, the	290
	lactic acid concentration was 10 g/l, and the initial pH was	291
	7. The only manipulation necessary during the experiments	292
	was stopping the shaker for ~8 min to connect the un-	293
	shaken flasks to the RAMOS device.	294
	Stress induced by lactic acid	295
	The stress induced by lactic acid was investigated by	296
	measuring the influence of different initial lactic acid	297
	concentrations: 1 g/l (0.51 osmol/l), 2.1 g/l (0.53 osmol/l),	298
	4.7 g/l (0.55 osmol/l), 9.6 g/l (0.72 osmol/l), 12.4 g/l	299
	(0.78 osmol/l), 13.7 g/l (0.81 osmol/l), 18.9 g/l	300
	(0.93 osmol/l), and 29.5 g/l (1.16 osmol/l) on respiration	301
	and growth of <i>C. glutamicum</i> . The numbers in parentheses	302
	are the calculated osmolarities of the entire medium. The	303
	lactic acid concentrations were determined with high-	304
	performance liquid chromatography (HPLC) analysis	305

306 (Dionex with RI and UV-VIS detectors, Dionex Sunnyvale,
 307 CA, USA) after adjusting the pH with NaOH to 7 and before
 308 inoculation. As stationary phase, an organic acid resin (CS
 309 Chromatography, Langerwehe, Germany) was used, while
 310 as eluent, it was a 1-mM H₂SO₄ with a flow rate of 0.6 ml/
 311 min. The column temperature was maintained at 30 °C.

312 To avoid oxygen limitation even at higher lactic acid
 313 concentrations, the RAMOS device was operated in the
 314 one-flow mode with a filling volume of 10 ml. After
 315 terminating the experiment, the final lactic acid concen-
 316 trations (HPLC), the final biomass concentrations (dry
 317 weight, OD), and the final pH were determined. During the
 318 fermentation, no manipulation was necessary.

319 Stress induced by osmolarity and pH

320 The stress induced by osmolarity and pH was investigated
 321 by comparing the respiration of two oxygen-unlimited
 322 batch cultures, one without buffering and the other with an
 323 MOPS buffer concentration of 42 g/l (0.2 M). The medium
 324 without buffer has an osmolarity of 0.73 osmol/l, which is
 325 increased by adding the buffer to 1 osmol/l. The filling
 326 volume was 10 ml, the lactic acid concentration was 10 g/l,
 327 and the initial pH was 7. The RAMOS device was operated
 328 in the two-phase mode. During the fermentation, no
 329 manipulation was necessary.

330 The growth characteristics of *C. glutamicum* at different
 331 initial pH was investigated by comparing respiration and
 332 biomass formation of unbuffered batch cultures with
 333 different initial pH of 4, 4.5, 5, 5.5, 7.1, 7.4, 8.5, 9, and
 334 9.5. The biomass and the pH measurements were
 335 performed in separate shake flasks with cotton plugs so
 336 as not to interrupt the OTR measurements. The filling
 337 volume was 10 ml and the lactic acid concentration was
 338 10 g/l. The RAMOS device was operated in the two-phase
 339 mode and stopped only twice for 10 min to take control
 340 samples. The shaker with the standard shake flasks was
 341 stopped 14 times for ~10 min to take samples (sample size
 342 0.15 ml).

343 Results

344 The applicability of respiration measurements in shake
 345 flasks to analyze the behavior of microorganisms during
 346 and after stress exposure was verified with the model
 347 system of *C. glutamicum* grown on the carbon source lactic
 348 acid. The organism was exposed to the stress factors such
 349 as carbon starvation, anaerobic conditions, lactic acid,
 350 osmolarity, and pH. Representative results are depicted in
 351 Figs. 1, 2, 3, 4, 5, 6, and 7. All experiments have been
 352 performed at least twice and minimum triple evidence was
 353 considered necessary to draw a conclusion.

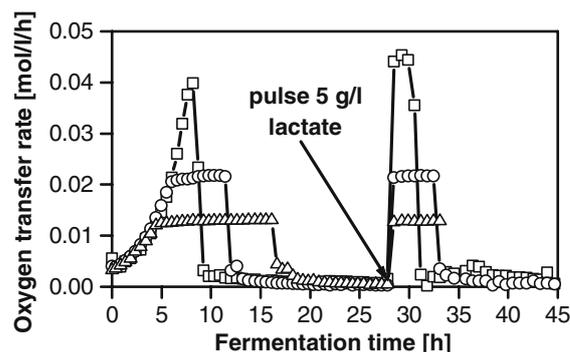


Fig. 1 Influence of carbon starvation on the metabolic activity of *C. glutamicum*. After an initial batch fermentation with a lactic acid concentration of 10 g/l, a pulse of 5 g/l lactic acid was added after 28 h. Culture conditions: 250 ml shake flask, filling volumes (before the pulse) 10 ml (□), 30 ml (○), 60 ml (△), shaking diameter 50 mm, shaking frequency 300 rpm, and initial pH 7

Stress induced by carbon starvation

The experiment was performed in three steps: first, the microorganisms were raised in a standard batch fermentation; second, they were exclusively carbon-starved (oxygen was continuously supplied) for 12–19 h depending on the culture conditions; third, the metabolic activity of the microorganisms was tested by adding a lactic acid pulse. Fig. 1 depicts the OTR over fermentation time of the entire experiment. The OTR curves reflect the experimental procedure. Initially, after inoculation, all cultures grew exponentially. The exponential growth continued until it was impaired by the OTR_{max}. The OTR_{max} depends only on the culture conditions (filling volume 10 ml oxygen-unlimited growth, and 30 and 60 ml oxygen-limited growth). After reaching OTR_{max}, the OTR stayed at a plateau until the carbon source was exhausted and then dropped sharply. With a decreasing OTR_{max}, the fermentation time increased. Then, after the drop, the OTR remained close to zero and the microorganisms were starving. Finally, after lactic acid was added, the OTR of the oxygen-limited cultures jumped to the level of the plateau before starvation. The OTR of the oxygen-unlimited culture exceeded even the maximum OTR reached in the initial batch, indicating the growth of the microorganisms after the pulse was added. After the renewed exhaustion of the carbon source, the OTR dropped again. In conclusion, a carbon starvation of up to 19 h does not influence the metabolic activity of *C. glutamicum*.

Stress induced by anaerobic conditions

The stress tolerance of *C. glutamicum* under anaerobic conditions was analyzed by comparing constantly aerobic batch cultures with temporarily anaerobic batch cultures. Fig. 2a (values are identical with the initial batch of Fig. 1) depicts the OTR of the constantly aerobic batch cultures over fermentation time. Fig. 2c depicts the OTR of the twice nitrogen-aerated batch cultures over fermentation time. The general culture characteristics were similar to the

Fig. 2 Influence of anaerobic conditions on the metabolic activity of *C. glutamicum*. **a** □, ○, and △. Continuous aeration with air. **b** Comparison of oxygen unlimited cultures with and without nitrogen aeration. **c** ■, ●, and ▲. After 4 and 7 h aeration for 1 h with nitrogen. **d** Comparison of oxygen-limited cultures with and without nitrogen aeration. **a, c** Actual fermentation time. **b, d** Nitrogen aeration time subtracted from actual fermentation time. Culture conditions: 250 ml shake flask; filling volumes 10 ml (□ and ■), 30 ml (○ and ●), 60 ml (△ and ▲); shaking diameter 50 mm; shaking frequency 300 rpm; lactic acid concentration 10 g/l; and initial pH 7

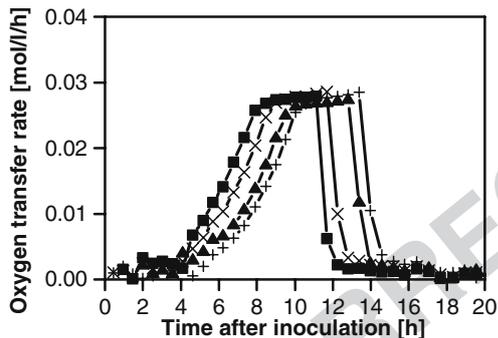
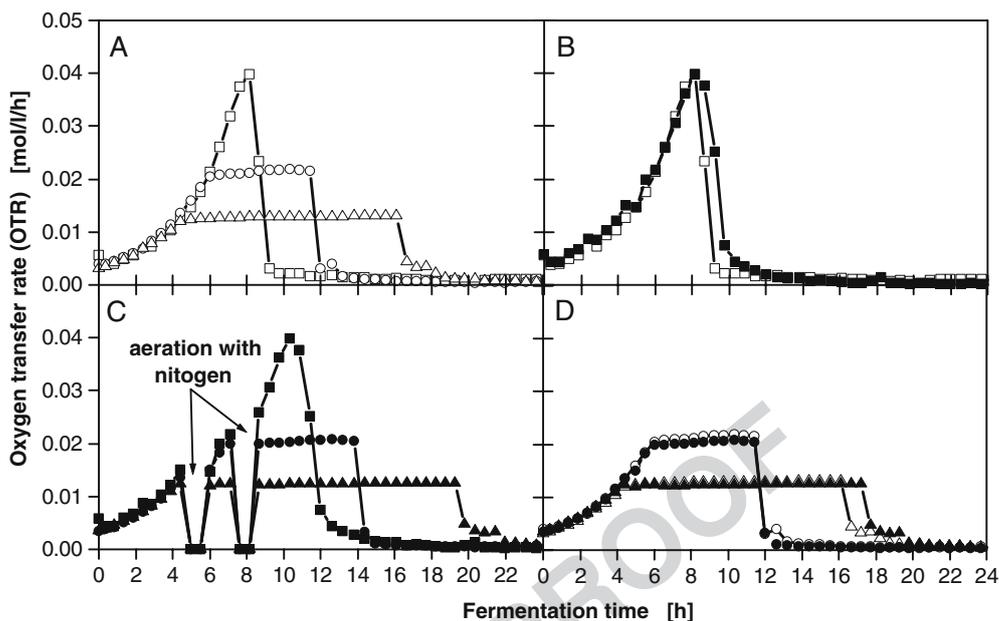


Fig. 3 Influence of a delayed aeration on the culture characteristics of *C. glutamicum*. After inoculation, the cultures were directly shaken (■), shaken after 1 h (×), shaken after 2 h (▲), and shaken after 3 h (+). Culture conditions: 250 ml shake flask, filling volume 25 ml, shaking diameter 50 mm, shaking frequency 300 rpm, lactic acid concentration 10 g/l, and initial pH 7

391 constantly aerobic batch. However, the fermentation time
 392 was prolonged and no growth occurred during the anaerobic
 393 periods. In a separate experiment (results not shown), it
 394 could be shown that the optical density as well of the culture
 395 did not increase during anaerobic conditions. A more detailed
 396 insight in the growth behavior of *C. glutamicum* after anaerobic
 397 stress is given in Fig 2b (oxygen-unlimited growth conditions,
 398 filling volume 10 ml) and Fig 2d (oxygen-limited growth conditions,
 399 filling volumes 30 and 60 ml). In both figures, the time of
 400 anaerobic fermentation (twice 1 h) is cut out from the data
 401 set shown in Fig. 2c to allow for a better comparison of the
 402 OTR curves. The cumulative consumed oxygen (integral of the
 403 OTR curve) was identical for oxygen-limited and oxygen-unlimited
 404 conditions, providing an oxygen substrate yield ($Y_{O_2/S}$) of
 405 $0.017 \text{ mol}_{O_2}/\text{g}_{\text{lactic acid}}$ with a standard deviation of
 406 $0.0016 \text{ mol}_{O_2}/\text{g}_{\text{lactic acid}}$. Also, the slope of the OTR and
 407 the whole course of the culture were not
 408

409 affected by the anaerobic conditions, proving that the
 410 metabolic activity of *C. glutamicum* is not affected by short
 411 periods of anaerobic conditions.

412 Similar observations were made with a second set of
 413 experiments. Anaerobic conditions were produced by delay-
 414 ing the shaking of the cultures after inoculation. Fig. 3
 415 depicts the OTR over time after inoculation. The general
 416 course of the OTR curves was independent of the shaking
 417 conditions reflecting the tolerance of *C. glutamicum* to
 418 anaerobic conditions. However, the exponential growth
 419 phases and the exhaustion of the carbon sources were shifted
 420 for 1, 2, and 3 h reflecting the delay of aeration after
 421 inoculation. If the OTR curves of Fig. 3 are superposed by
 422 cutting out the unshaken periods, the OTR curves are
 423 nearly identical (figure not shown). In conclusion, during
 424 short anaerobic periods, *C. glutamicum* falls in a state of
 425 dormancy. Similar to sleep, we define dormancy as a state
 426 where the microorganisms have no or only very reduced
 427 metabolic activity without growth; however, the ability to
 428 be metabolically active and grow is not significantly
 429 reduced.

Stress induced by lactic acid

430
 431 The stress induced by varying acid concentrations (Fig. 4)
 432 was investigated by comparing the OTR of batch cultures
 433 with initial lactic acid concentrations ranging from 1 g/l
 434 (0.01 mol/l) to 29.5 g/l (0.33 mol/l) at a constant initial pH
 435 of 7. Because the pH was always above 7 (Fig. 4d), lactic
 436 acid (pK_a 3.86) was entirely present in the dissociated
 437 form. Up to a concentration of 10 g/l (Fig. 4a), the lactic
 438 acid concentration did not influence the slope of the OTR,
 439 and at higher concentrations (Fig. 4c), the slope decreased
 440 due to lactic acid inhibition.

441 In aerobic cultures, almost every physiological activity is
 442 reflected by the OTR (Anderlei et al. 2004; Anderlei and

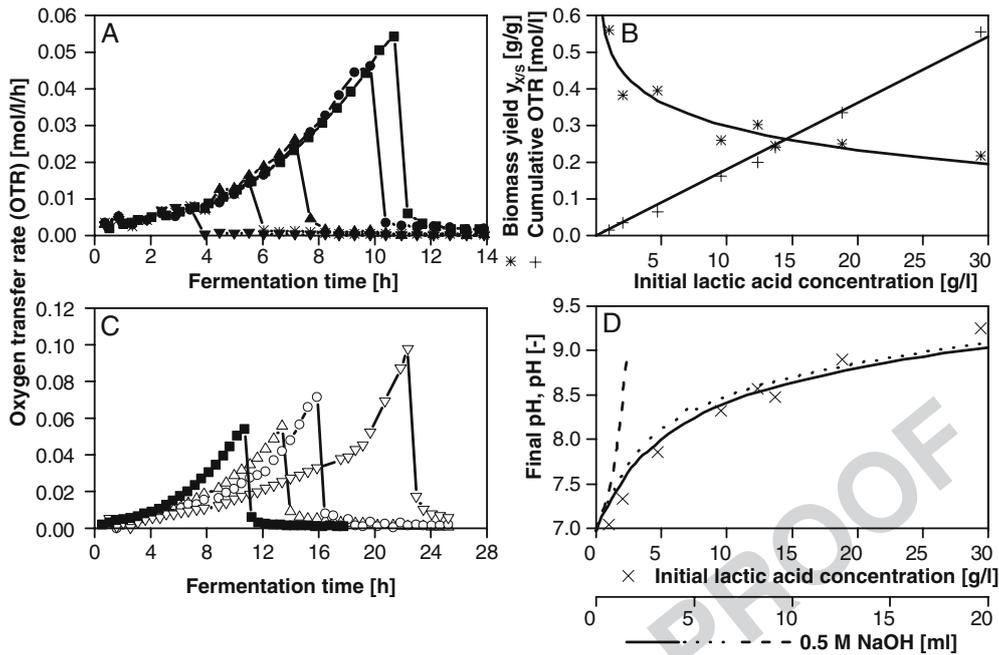


Fig. 4 Influence of different initial lactic acid concentrations on respiration and growth of *C. glutamicum*. **a** Oxygen transfer rate (OTR) over fermentation time, low initial lactic acid concentrations 1 g/l (▼), 2.1 g/l (*), 4.7 g/l (▲), 9.6 g/l (●), and 12.4 g/l (■). **b** Cumulative consumed oxygen over initial lactic acid concentration (+), and biomass substrate yield over initial lactic acid concentration (*). **c** OTR over fermentation time, high initial lactic acid concentrations 12.4 g/l (■), 13.7 g/l (△), 18.9 g/l (○), and

29.5 g/l (▽). **d** Final pH over initial lactic acid concentration (×). Titration curves normalized to pH 7 as described in the “Materials and methods” section over added amount titrant NaOH: standard medium (—), medium without lactic acid (·····), and medium without ammonium sulfate (—). Culture conditions: 250 ml shake flask, filling volume 10 ml, shaking diameter 50 mm, shaking frequency 300 rpm, and initial pH 7

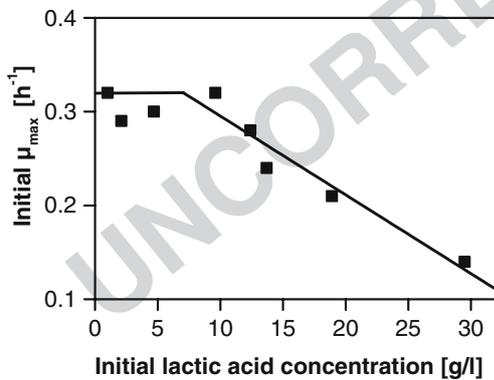


Fig. 5 Initial maximum growth rate (μ_{max}) at different initial lactic acid concentrations. The initial μ_{max} were derived from the slopes of the oxygen transfer rate (OTR) depicted in Fig. 4a,c. OTR values with a fermentation time between 2.5 and 6 h were used to calculate the initial μ_{max}

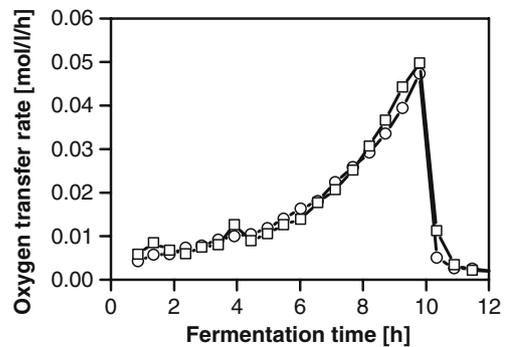


Fig. 6 Influence of buffer on the growth of *C. glutamicum*. Medium without buffer (○), and medium with 42 g/l MOPS buffer (□). Culture conditions: 250 ml shake flask, filling volume 10 ml, shaking diameter 50 mm, shaking frequency 300 rpm, lactic acid concentration 10 g/l, initial pH 7, and final pH 8.4 (unbuffered) and 7.6 (buffered)

443 Büchs 2000; Losen et al. 2004; Stöckmann et al. 2003).
 444 Thus, in most cases, it is possible to derive the growth rate
 445 of a biological culture from the slope of the OTR as
 446 described by Stöckmann et al. (2003). Using the slopes of
 447 the OTR curves depicted in Fig. 4a,c, it was possible to
 448 identify three growth phases. At fermentation times of less
 449 than 2.5 h, *C. glutamicum* showed an acceleration phase.
 450 As depicted in Fig. 5 at fermentation times between 2.5 and
 451 6 h, pH values below 8, and initial lactic acid concentra-
 452 tions of less than 10 g/l, the microorganisms grew with the

maximum growth rate of 0.3–0.32 h⁻¹. At higher initial
 lactic acid concentrations [*i*C₃H₆O₃ (g/l)], the growth rate
 $[\mu \text{ (h}^{-1}\text{)}]$ decreased linearly with increasing initial lactic
 acid concentration [$\mu = 0.38 - 0.0084 \cdot iC_3H_6O_6$, $R^2 = 0.92$,
 10 g/l $\leq iC_3H_6O_6 \leq 30$ g/l]. During the late batch phase,
 when the lactic acid concentration was low, and the pH
 value was above 8, the growth rate ($\mu = 0.235 \text{ h}^{-1}$, standard
 deviation $\sigma = 0.016 \text{ h}^{-1}$, $iC_3H_6O_3 \geq 10$ g/l) was independent
 of the initial lactic acid concentration.

453
 454
 455
 456
 457
 458
 459
 460
 461

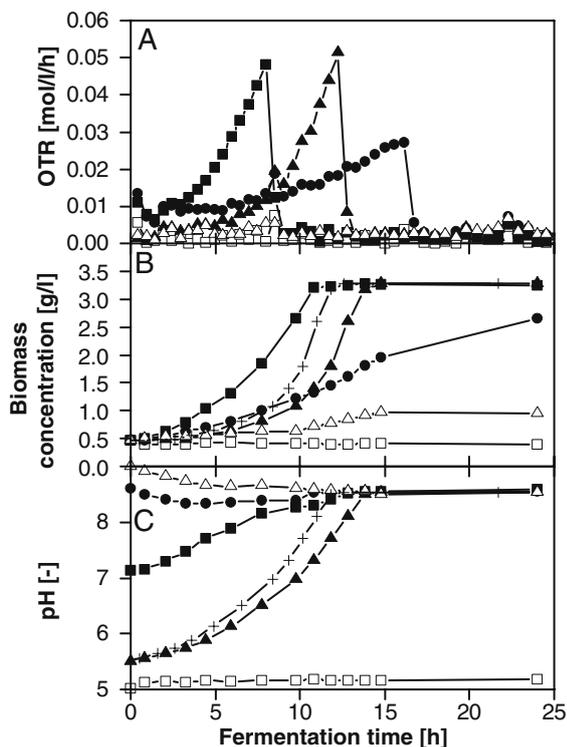


Fig. 7 Influence of different initial pH values of 5 (□), 5.5 (▲), 7.1 (■), 8.5 (●), and 9 (△) on respiration and growth of *C. glutamicum*. **a** Oxygen transfer rate (OTR), **b** Biomass concentration, **c** pH, **b, c** + Initial pH 5.5, the time of interruptions of the shaker is subtracted from the fermentation time. Culture conditions: 250 ml shake flask, filling volume 10 ml, shaking diameter 50 mm, shaking frequency 300 rpm, and lactic acid concentration 10 g/l

462 Fig. 4b depicts the biomass substrate yield coefficient
 463 ($Y_{X/S}$) and the cumulative consumed oxygen, which is the
 464 integral of the OTR curve from the time of inoculation to the
 465 time of the maximum OTR, over the initial lactic acid
 466 concentration. The biomass substrate yield decreased with
 467 increasing lactic acid concentration. The cumulative con-
 468 sumed oxygen, however, increased linearly with the initial
 469 lactic acid concentration giving a constant oxygen substrate
 470 yield ($Y_{O_2/S} = 0.017 \text{ mol}_{O_2}/\text{g}_{\text{lactic acid}}$, standard deviation
 471 $\sigma = 0.0015 \text{ mol}_{O_2}/\text{g}_{\text{lactic acid}}$).

472 The consumption of the acid lactic acid leads to an
 473 increase of the pH value. Fig. 4d depicts the final pH
 474 (points) reached by cultures with different initial lactic acid
 475 concentrations. The measured increase of the pH values
 476 depends on the initial lactic acid concentration and on the
 477 buffering capacity of the media. Titration curves of the
 478 medium were used as a simple tool to describe the final pH
 479 value of the biological cultures and to identify the buffering
 480 effect of the different medium components. Fig. 4d depicts
 481 the titration curves (lines) of the standard medium as
 482 described in the "Materials and methods" section, of a
 483 medium without lactic acid, and of a medium without
 484 $(\text{NH}_4)_2\text{SO}_4$. The titration curves of the media with and
 485 without lactic acid are nearly identical, affirming that the
 486 consumption of lactic acid (pK_a 3.86) cannot influence

the buffering capacity of the medium at pH above 7. The
 titration curve of the medium without $(\text{NH}_4)_2\text{SO}_4$ is much
 steeper, showing the buffering effect of ammonium sulfate
 (pK_a 9.25). Titration curves of a medium without phos-
 phates (results not shown) showed that the phosphates (pK_a
 7.2) have only a small influence, proving that the excess
 amount of ammonium present in the medium is responsible
 for the relatively moderate pH increase at high initial
 lactate concentrations.

In conclusion, initial lactic acid concentrations up to
 10 g/l do not influence the growth of *C. glutamicum*. At
 higher concentrations up to 30 g/l, the growth rate de-
 creases linearly with the lactic acid concentration. With
 increasing lactic acid concentration, the biomass substrate
 yield decreases, without affecting the oxygen substrate
 yield. The final pH reached by batch cultures with different
 initial lactic acid concentrations followed the titration curve
 of the medium.

Stress induced by osmolarity and pH

Fig. 6 depicts the OTR over fermentation time of oxygen-
 unlimited unbuffered and buffered batch cultures. Both
 cultures had an initial pH of 7. The pH of the unbuffered
 and buffered cultures increased to 8.4 and 7.6, respectively.
 Up to a fermentation time of 8 h, both cultures had the same
 slope, demonstrating that the increased osmolarity does not
 influence the growth of *C. glutamicum*. At fermentation
 times exceeding 8 h, the growth rate of the unbuffered
 culture decreased. The buffered culture continued to grow
 with the maximum growth rate.

The effect of different initial pH on growth and
 respiration of *C. glutamicum* was investigated by compar-
 ing OTR and growth curves of unbuffered batch cultures
 with initial pH ranging from 4 to 9.5. Fig. 7 depicts the
 OTR (Fig. 7a), the biomass concentration (Fig. 7b), and the
 pH (Fig. 7c) over the fermentation time of cultures with
 different initial pH. The response of *C. glutamicum* to
 different initial pH values can be classified in three groups.
 The first group includes the initial pH values of 7.1 (6.4 and
 7.4 results not shown). The OTR and growth curves of this
 group were nearly identical; they increased exponentially.
 The pH changed from its initial value to 8.5. The second
 group showed a reduced metabolic activity and includes
 the initial pH values of 5.5 and 8.5. Due to pH inhibition,
 the cultures of this group showed a prolonged fermentation
 time and a reduced growth rate. The culture with an initial
 pH of 5.5 had a reduced OTR and growth rate at the
 beginning. However, with increasing pH, the slope became
 equal to the first group. In contrast, the OTR curve with an
 initial pH of 8.5 had an equal OTR at the beginning. The
 slope, however, stayed low for the entire fermentation time.
 The third group includes the initial pH values of 5 and 9 (4,
 4.5 and 9.5 results not shown). None of the cultures of this
 group showed any considerable metabolic activity. The
 OTRs remained close to zero, the biomass concentrations
 did not or only slightly increase, and the pH values stayed
 at their initial values. However, from the final pH values

543 reached by the cultures with a high initial lactic acid
544 concentration (Fig. 4d), it can be concluded that *C.*
545 *glutamicum* can grow with high growth rates at pH up to
546 9 if the microorganisms have time to adapt. Small de-
547 creases of the pH at high initial pH (Fig. 7c) are probably
548 caused by the gassing out of NH₃ at pH close to the pK_a
549 (9.25).

550 The OTR curves (Fig. 7a) reached the stationary phase
551 earlier than the biomass (Fig. 7b) and pH (Fig. 7c) curves.
552 During the respiration measurements, the shaker was
553 stopped only twice for 10 min to take samples; however,
554 the shaker for the biomass and pH determination was
555 stopped 14 times for 10 min to take samples. If the inter-
556 ruptions of the shaker are subtracted from the fermentation
557 time (Fig. 7b,c only demonstrated for the culture with a pH
558 value of 5.5), the fermentation time of the OTR curves
559 (Fig. 7a) match the fermentation time of the biomass and
560 pH curves (Fig. 7b,c). Probably, stopping the shaker to take
561 samples leads to short anaerobic periods, which freeze
562 growth and metabolic activity. The observed influence of
563 the interruptions of the shaker on the fermentation time
564 confirms the conclusions drawn before about the stress
565 induced by anaerobic conditions.

566 It can be concluded that the increased osmolarity of up to
567 1 osmol/l caused by the buffer does not affect the growth or
568 respiration of *C. glutamicum*. Initial pH values ranging
569 from 6.4 to 7.4 lead to uninhibited growth. Without adap-
570 tation, the organism did not grow at pH_≤5 or pH_≥9, but
571 with adaptation, growth was observed up to a pH of 9.

572 Discussion

573 Stress induced by carbon starvation

574 With respiration measurement in shake flasks, it was
575 shown that a starvation time of 19 h does not reduce the
576 metabolic activity of *C. glutamicum* grown on lactic acid.
577 The starvation time used in this study can be sufficient to
578 reduce the viability of Gram-positive organisms. For
579 example, Ferreira et al. (2001) observed for *L. mono-*
580 *cytogenes* (WT) a 25% decrease in viability over a
581 starvation time of 12 h. Other Gram-positive organisms
582 like *M. tuberculosis* show a high resistance to carbon
583 starvation. With plate counts, Primm et al. (2000) found no
584 loss in viability of *M. tuberculosis* for 106 days. The high
585 resistance against carbon starvation of *C. glutamicum*
586 observed in this study probably results from the complex
587 starvation-survival strategies of *C. glutamicum* (Wehmeier
588 et al. 1998, 2001), which are similar to the ones of *M.*
589 *tuberculosis* (Primm et al. 2000).

590 Stress induced by anaerobic conditions

591 In this study, it was found that during short anaerobic
592 periods, *C. glutamicum* on lactic acid falls in a state of
593 dormancy, without growth and without a loss in metabolic
594 activity. The behavior of *C. glutamicum* under anaerobic

595 conditions on lactic acid has so far not been investigated.
596 On glucose, Inui et al. (2004) observed no growth under
597 oxygen-deprived conditions, but a continuous formation of
598 lactate and succinate. For *M. tuberculosis* on complex
599 medium, Primm et al. (2000) found only a slight decrease
600 in viability over a 23-week anaerobic period. Kim et al.
601 (2005) describes genes involved in oxidative stress pro-
602 tection of *C. glutamicum*.

603 Stress induced by lactic acid

604 In this study, it was found that lactic acid present in the
605 dissociated form (Figs. 4 and 5) had no influence on the
606 growth of *C. glutamicum* up to an initial concentration of
607 10 g/l (0.11 M). At higher concentrations of up to 30 g/l
608 (0.33 M), the growth rate decreased linearly with the lactic
609 acid concentration. Coccain et al. (1993) observed for
610 *C. glutamicum* no influence of initial lactate concentrations
611 on the growth rate between 0.035 and 0.125 M. According
612 to Houtsma et al. (1996), the dissociated form of lactate
613 leads to a linear decrease of the growth rate of *L. innocua* at
614 concentrations between 0.25 and 1.1 M. Above 1.25 M, the
615 growth of *L. innocua* is completely inhibited. According to
616 the review of Presser et al. (1997), the growth of various
617 organisms is completely inhibited by the dissociated form
618 of organic acids at concentrations between 0.1 and 0.8 M.

619 In this study, it was observed that with increasing lactic
620 acid concentration, the biomass substrate yield ($Y_{X/S}$)
621 decreases. For *C. glutamicum*, decreasing growth rates
622 combined with decreasing biomass substrate yields under
623 stress conditions were observed by Guillouet and Engasser
624 (1995). $Y_{X/S}$ between 0.36 and 0.62 g_{biomass}/g_{lactate}
625 depending on the growth rate and mode of operation
626 were observed by Coccain-Bousquet and Lindley (1995)
627 and Coccain et al. (1993), but were not attributed to stress
628 conditions. The oxygen substrate yield ($Y_{O_2/S}$) of 0.017
629 mol_{O₂}/g_{lactic acid} observed in this study is identical to the
630 one reported (Coccain-Bousquet and Lindley 1995) for
631 continuous cultures under conditions where the substrate is
632 entirely consumed ($Y_{O_2/S}$ was calculated from the data
633 depicted in the figures). The question on why the biomass
634 substrate yield decreases with increasing lactic acid con-
635 centration, while the oxygen substrate yield stays constant,
636 could not yet be explained. However, it may be caused by
637 the formation of an undetected byproduct, or by a sig-
638 nificant change in biomass composition.

639 Stress induced by osmolarity

640 In this study, an osmolarity of 1 osmol/l had no influence
641 on the growth of *C. glutamicum*. This agrees with Rönisch
642 (2000), who found the same results for osmolalities up to
643 2.0 osmol/kg for *C. glutamicum* on sucrose, but noticed a
644 decreased growth rate at 2.5 osmol/kg. By increasing the
645 osmolality from 0.4 to 2 osmol/kg for *C. glutamicum* on
646 glucose, Guillouet and Engasser (1995) observed a reduc-

647 tion of the growth rate from 0.7 to 0.2 h⁻¹ and a reduction
 648 of the biomass substrate yield coefficient from 0.6 to
 649 0.3 g_{biomass}/g_{glucose}. The high tolerance of *C. glutamicum*
 650 against osmotic stress makes it unlikely, that the observed
 651 reduction of the growth rate with increased initial lactic
 652 acid concentration (10 g/l, 0.73 osmol/l; 30 g/l, 1.17 osmol/
 653 l) is caused by the increased osmolarity. The high tolerance
 654 of *C. glutamicum* against osmotic stress is caused by the
 655 possibilities of the organism to sense osmolarity and to
 656 take up and produce compatible solutes for protection
 657 (Guillouet and Engasser 1995, 1996; Peter et al. 1998;
 658 Skjerdal et al. 1996; Varela et al. 2003; Wolf et al. 2003).

659 Stress induced by pH

660 In this study, initial pH values ranging from 6.4 to 7.4 lead
 661 to uninhibited growth of *C. glutamicum*. Without adapta-
 662 tion, the organism did not grow at pH≤5 or pH≥9. With
 663 adaptation, however, growth was observed up to a pH of 9.
 664 Similar results were reported by Shah et al. (2002), who
 665 found lysine production of *C. glutamicum* from pH 6 to 9
 666 with a maximum at pH 7.5. Bröer and Krämer (1991)
 667 analyzed the influence of external pH on lysine efflux and
 668 found a maximum at pH 7.8. The importance of adaptation
 669 for acid tolerance of Gram-positive organisms has been
 670 reported (Bodmer et al. 2000; Cotter and Hill 2003;
 671 O'Driscoll et al. 1996; Saklani-Jusforgues et al. 2000).

672 With the chosen measuring set-up, it is not possible to
 673 distinguish whether the observed growth inhibition of
 674 *C. glutamicum* at low pH is caused by the pH itself or by
 675 the undissociated form of the lactic acid. The undissociated
 676 form of lactic acid is believed to have a higher inhibitory
 677 effect (Cotter and Hill 2003; Salmond et al. 1984; Shelef
 678 1994) than the dissociated form. At pH 5.5 and 5, about
 679 0.0025 and 0.0075 M of the lactic acid (total concentration
 680 0.11 M), respectively, were present in the undissociated
 681 form. Presser et al. (1997, 1998) observed for *E. coli* a
 682 complete inhibition of growth at undissociated lactate
 683 concentrations exceeding 0.0083 M regardless of the pH or
 684 the total lactate concentration. Houtsma et al. (1996)
 685 observed a total inhibition of *L. innocua* at pH 5.5 with a
 686 lactate concentration of 0.2 M of which 0.0045 M was
 687 undissociated.

688 Evaluation of the general method

689 In this study, we demonstrated the broad applicability of
 690 respiration measurements in shake flasks to study the
 691 behavior of *C. glutamicum* during and after exposure to
 692 stress. Experimental procedures were developed to study
 693 the following stress factors: carbon starvation, anaerobic
 694 conditions, organic acids, osmolarity, and pH. Similar
 695 procedures may be applied to study the response of micro-
 696 organisms to stress factors like heat, oxygen, antibiotics,
 697 hormones, antibodies, or starvation of nitrogen, phospho-
 698 rus, amino acids, or trace elements. The importance to run
 699 stress-response analysis without interferences during the

cultivation was demonstrated by showing the influence,
 which inevitable interruptions of the shaker had when
 samples were taken. The short periods without agitation,
 necessary to transfer samples to new culture vessels or
 measuring devices, like respirometers, may lead to detri-
 mental anaerobic conditions. Furthermore, if evidence
 exists, that the microorganisms show a different growth
 behavior in liquid cultures than on plates, respiration mea-
 surement in shake flasks is recommended.

The duration of the measuring cycle of the RAMOS
 device may limit the applicability of the method. The
 standard duration of the measuring cycle is 30 min, which
 can be reduced for strongly respiring cultures to 10 min.
 This is sufficient for most stress-response analysis because
 activity losses after exposure to stress mainly occur within
 hours or days. The new possibility to study the stress
 response of microorganisms in online-monitored shake
 flasks makes it possible to study several cultures simulta-
 neously, and increases the possible number of experiments.
 The high throughput combined with the possibility to
 perform the entire experiment in the same culture vessel
 and in the same medium makes the respiration measure-
 ment in shake flasks an important tool for research and
 industrial process optimization.

Acknowledgements We thank Dipl.-Ing. Karen Otten and Prof.
 Dr.-Ing. Horst R. Maier from the institute for ceramic components in
 mechanical engineering from RWTH Aachen University for their
 help and advice. This work was supported by a grant from the
 German Research Foundation (DFG).

References

- Anderlei T, Büchs J (2000) Device for sterile online measurement of
 the oxygen transfer rate in shaking flasks. *Biochem Eng J*
 7:157–162
- Anderlei T, Zang W, Papaspyrou M, Büchs J (2004) Online
 respiration activity measurement (OTR, CTR, RQ) in shake
 flasks. *Biochem Eng J* 17:187–194
- Barreiro C, González-Lavado E, Pátek M, Martín J-F (2004)
 Transcriptional analysis of the *groES-groEL1*, *groEL2*, and
dnaK genes in *Corynebacterium glutamicum*: characterization
 of heat shock-induced promoters. *J Bacteriol* 186:4813–4817
- Barreiro C, González-Lavado E, Brand S, Tauch A, Martín J-F
 (2005) Heat shock proteome analysis of wild-type *Corynebacterium glutamicum* ATCC 13032 and a spontaneous mutant lacking *groEL1*, a dispensable chaperone. *J Bacteriol* 187:884–889
- Bodmer T, Miltner E, Bermudez LE (2000) *Mycobacterium avium* resists exposure to the acidic conditions of the stomach. *FEMS Microbiol Lett* 182:45–49
- Breidt F Jr, Hayes JS, McFeeters RF (2004) Independent effects of acetic acid and pH on survival of *Escherichia coli* in simulated acidified pickle products. *J Food Prot* 67:12–18
- Bröer S, Krämer R (1991) Lysine excretion by *Corynebacterium glutamicum* 1. Identification of a specific secretion carrier system. *Eur J Biochem* 202:131–135
- Burkovski A (2003) I do it my way: regulation of ammonium uptake and ammonium assimilation in *Corynebacterium glutamicum*. *Arch Microbiol* 179:83–88
- Cocaign-Bousquet M, Lindley ND (1995) Pyruvate overflow and carbon flux within the central metabolic pathways of *Corynebacterium glutamicum* during growth on lactate. *Enzyme Microb Technol* 17:260–267

700
701
702
703
704
705
706
707
708
709
710
711
712
713
714
715
716
717
718
719
720
721
722
723
724
725
726
727
728
729
730
731
732
733
734
735
736
737
738
739
740
741
742
743
744
745
746
747
748
749
750
751
752
753
754
755
756
757
758
759
760

- 761 Cocaign M, Monnet C, Lindley ND (1993) Batch kinetics of
762 *Corynebacterium glutamicum* during growth on various carbon
763 substrates: use of mixtures to localize metabolic bottlenecks.
764 Appl Microbiol Biotechnol 40:526–530
- 765 Cotter PD, Hill C (2003) Surviving the acid test: responses of gram-
766 positive bacteria to low pH. Microbiol Mol Biol Rev 67:
767 429–453
- 768 Ferreira A, O'Byrne CP, Boor KJ (2001) Role of σ^B in heat, ethanol,
769 acid, and oxidative stress resistance and during carbon starva-
770 tion in *Listeria monocytogenes*. Appl Environ Microbiol 67:
771 4454–4457
- 772 Gourdon P, Baucher M-F, Lindley ND, Guyonvarch A (2000)
773 Cloning the malic enzyme gene from *Corynebacterium*
774 *glutamicum* and role of the enzyme in lactate metabolism.
775 Appl Environ Microbiol 66:2981–2987
- 776 Guillouet S, Engasser JM (1995) Growth of *Corynebacterium*
777 *glutamicum* in glucose-limited continuous cultures under high
778 osmotic pressure. Influence of growth rate on the intracellular
779 accumulation of proline, glutamate, and trehalose. Appl
780 Microbiol Biotechnol 44:496–500
- 781 Guillouet S, Engasser JM (1996) Growth of *Corynebacterium*
782 *glutamicum* in ammonium- and potassium-limited continuous
783 cultures under high osmotic pressure. Appl Microbiol Biotech-
784 nol 46:291–296
- 785 Gutmann M, Hoischen C, Krämer R (1992) Carrier-mediated
786 glutamate secretion by *Corynebacterium glutamicum* under
787 biotin limitation. Biochim Biophys Acta 1112:115–123
- 788 Gruber TM, Bryant DA (1997) Molecular systematic studies of
789 eubacteria, using σ^{70} -type sigma factors of group 1 and group
790 2. J Bacteriol 179:1734–1747
- 791 Houtsma PC, Kant-Muermans ML, Rombouts FM, Zwietering MH
792 (1996) Model for the combined effects of temperature, pH, and
793 sodium lactate on growth rates of *Listeria innocua* in broth and
794 bologna-type sausages. Appl Environ Microbiol 62:1616–1622
- 795 Hu Y, Coates ARM (1999) Transcription of two sigma 70 homo-
796 logue genes, *sigA* and *sigB*, in stationary-phase *Mycobacterium*
797 *tuberculosis*. J Bacteriol 181:469–476
- 798 Ihssen J, Egli T (2004) Specific growth rate and not cell density
799 controls the general stress response in *Escherichia coli*.
800 Microbiology 150:1637–1648
- 801 Inui M, Muratami S, Okino S, Kawaguchi H, Vertès AA, Yukawa H
802 (2004) Metabolic analysis of *Corynebacterium glutamicum*
803 during lactate and succinate productions under oxygen depri-
804 vation conditions. J Mol Microbiol Biotechnol 7:182–196
- 805 Ishige T, Krause M, Bott M, Wendisch VF, Sahn H (2003) The
806 phosphate starvation stimulon of *Corynebacterium glutamicum*
807 determined by DNA microarray analyses. J Bacteriol 185:
808 4519–4529
- 809 Kim T-H, Park J-S, Kim H-J, Kim Y, Kim P, Lee H-S (2005) The
810 *whcE* gene of *Corynebacterium glutamicum* is important for
811 survival following heat and oxidative stress. Biochem Biophys
812 Res Commun 337:757–764
- 813 Kinoshita S, Udaka S, Shimono M (1957) Amino acid fermentation.
814 I. Production of L-glutamic acid by various microorganisms.
815 J Gen Appl Microbiol 3:193–205
- 816 Kočan M, Schaffer S, Ishige T, Sorger-Hermann U, Wendisch VF,
817 Bott M (2006) Two-component systems of *Corynebacterium*
818 *glutamicum*: deletion analysis and involvement of the PhoS-
819 PhoR system in the phosphate starvation response. J Bacteriol
820 188:724–732
- 821 Koffas MAG, Jung GY, Stephanopoulos G (2003) Engineering
822 metabolism and product formation in *Corynebacterium gluta-*
823 *micum* by coordinated gene overexpression. Metab Eng 5:
824 32–41
- 825 Losen M, Lingen B, Pohl M, Büchs J (2004) Effect of oxygen-
826 limitation and medium composition on *Escherichia coli* in
827 small-scale cultures. Biotechnol Prog 20:1062–1068
- 828 Maier U, Büchs J (2001) Characterisation of the gas-liquid mass
829 transfer in shaking bioreactors. Biochem Eng J 7:99–106
- 830 Maier U, Losen M, Büchs J (2004) Advances in understanding and
831 modeling the gas-liquid mass transfer in shake flasks. Biochem
832 Eng J 17:155–167
- Mandel MJ, Silhavy TJ (2005) Starvation for different nutrients in
Escherichia coli results in differential modulation of RpoS
levels and stability. J Bacteriol 187:434–442
- Mrotzek C, Andertei T, Henzler H-J, Büchs J (2001) Mass transfer
resistance of sterile plugs in shaking bioreactors. Biochem Eng
J 7:107–112
- Nolden L, Ngoutou-Nkili C-E, Bendt AK, Krämer R, Burkovski A
(2001) Sensing nitrogen limitation in *Corynebacterium gluta-*
micum: the role of *glnK* and *glnD*. Mol Microbiol 42:
1281–1295
- O'Driscoll B, Grahan CG, Hill C (1996) Adaptive acid tolerance
response in *Listeria monocytogenes*: isolation of an acid-
tolerant mutant which demonstrates increased virulence. Appl
Environ Microbiol 62:1693–1698
- Peter H, Weil B, Burovski A, Krämer R, Morbach S (1998)
Corynebacterium glutamicum is equipped with four secondary
carriers for compatible solutes: identification, sequencing, and
characterization of the proline/ectoine/glycine betaine carrier,
EctP. J Bacteriol 180:6005–6012
- Presser KA, Ratkowsky DA, Ross T (1997) Modeling the growth
rate of *Escherichia coli* as a function of pH and lactic acid
concentration. Appl Environ Microbiol 63:2355–2360
- Presser KA, Ross T, Ratkowsky DA (1998) Modeling the growth
limits (growth/no growth interface) of *Escherichia coli* as a
function of temperature, pH, lactic acid concentration, and
water activity. Appl Environ Microbiol 64:1773–1779
- Primm TP, Andersen SJ, Mizrahi V, Avarbock DA, Rubin H, Barry
CE (2000) The stringent response of *Mycobacterium tuber-*
culosis is required for long-term survival. J Bacteriol 182:
4889–4898
- Roe AJ, O'Byrne C, McLaggan D, Booth IR (2002) Inhibition of
Escherichia coli growth by acetic acid: a problem with
methionine biosynthesis and homocysteine toxicity. Microbi-
ology 148:2215–2222
- Rönsch H (2000) Untersuchung zum Einfluss der Osmoregulation
auf die Aminosäureproduktion mit *Corynebacterium glutami-*
cum. Ph.D. Thesis, University Cologne, Germany
- Ross T, Ratkowsky DA, Mellefont LA, McMeekin TA (2003)
Modelling the effects of temperature, water activity, pH and
lactic acid concentration on the growth rate of *Escherichia coli*.
Int J Food Microbiol 82:33–43
- Saklani-Jusforgues H, Fontan E, Goossens PL (2000) Effect of acid-
adaptation on *Listeria monocytogenes* survival and transloca-
tion in a murine intragastric infection model. FEMS Microbiol
Lett 193:155–159
- Salmond CV, Kroll RG, Booth IR (1984) The effect of food
preservatives on pH homeostasis in *Escherichia coli*. J Gen
Microbiol 130:2845–2850
- Shah AH, Hameed A, Ahmad S, Khan GM (2002) Optimization of
culture conditions for L-lysine fermentation by *Corynebacteri-*
um glutamicum. Online J Biol Sci 2:151–156
- Shelef LA (1994) Antimicrobial effects of lactate: a review. J Food
Prot 57:445–450
- Silberbach M, Schäfer M, Hüser AT, Kalinowski J, Pühler A,
Krämer R, Burkovski A (2005) Adaptation of *Corynebacterium*
glutamicum to ammonium limitation: a global analysis using
transcriptome and proteome techniques. Appl Environ Micro-
biol 71:2391–2402
- Skjerdal OT, Sletta H, Flenstad SG, Josefsen KD, Levine DW,
Ellingsen TE (1996) Changes in intracellular composition in
response to hyperosmotic stress of NaCl, sucrose, or glutamic
acid in *Brevibacterium lactofermentum* and *Corynebacterium*
glutamicum. Appl Microbiol Biotechnol 44:635–642
- Stansen C, Uy D, Delaunay S, Eggeling L, Goergen J-L, Wendisch
VF (2005) Characterization of a *Corynebacterium glutamicum*
lactate utilization operon induced during temperature-triggered
glutamate production. Appl Environ Microbiol 71:5920–5928
- Stöckmann C, Maier U, Anderlei T, Knocke C, Gellissen G, Büchs J
(2003) The oxygen transfer rate as key parameter for the
characterization of *Hansenula polymorpha* screening cultures.
J Ind Microbiol Biotechnol 30:613–622

- 904 Varela C, Agosin E, Baez M, Klapa M, Stephanopoulos G (2003) 915
905 Metabolic flux redistribution in *Corynebacterium glutamicum* 916
906 in response to osmotic stress. *Appl Microbiol Biotechnol* 917
907 60:547–555 918
- 908 Watson SP, Clements MO, Foster SJ (1998) Characterization of the 919
909 starvation-survival response of *Staphylococcus aureus*. 920
910 *J Bacteriol* 180:1750–1758 921
- 911 Wehmeier L, Schäfer A, Burkovski A, Krämer R, Mechold U, 922
912 Malke H, Pühler A, Kalinowski J (1998) The role of the 923
913 *Corynebacterium glutamicum rel* gene in (p)ppGpp metabo- 924
914 lism. *Microbiology* 144:1853–1862 925
- Wehmeier L, Brockmann-Gretza O, Pisabarro A, Tauch A, Pühler A, 915
Martin JF, Kalinowski J (2001) A *Corynebacterium glutami-* 916
cum mutant with a defined deletion within the *rplK* gene is 917
impaired in (p)ppGpp accumulation upon amino acid starva- 918
tion. *Microbiology* 147:691–700 919
- Wendisch VF, DeGraaf AA, Sahm H, Eikmanns BJ (2000) 920
Quantitative determination of metabolic fluxes during coutili- 921
zation of two carbon sources: comparative analyses with 922
Corynebacterium glutamicum during growth on acetate and/or 923
glucose. *J Bacteriol* 182:3088–3096 924
- Wolf A, Krämer R, Morbach S (2003) Three pathways for trehalose 925
metabolism in *Corynebacterium glutamicum* ATCC 13032 and 926
their significance in response to osmotic stress. *Mol Microbiol* 927
49:1119–1134 928

UNCORRECTED PROOF

AUTHOR QUERY FORM

<p>Journal Code: [253] Article Number: [436]</p>	<p>Please e-mail your responses together with your list of corrections, or send the completed form and your marked proof to: Springer Proof Corrections SPI Technologies PITC Building, Pascor Drive, Sto Nino, Paranaque City 1700, Philippines fax: +63-2-325-0428; +63-2-325-0430 Tel.: +63-2-855-8763 e-mail: proofcorrections@sps-spitech.com</p>
---	--

Dear Author,

During the preparation of your manuscript for typesetting, some questions have arisen. These are listed below. Please check your typeset proof carefully and mark any corrections in the margin of the proof or compile them as a separate list.

Bibliography

If discrepancies were noted between the literature list and the text references, the following may apply:

- 1 The references listed below were noted in the text but appear to be missing from your literature list. Please complete the list or remove the references from the text.
- 2 *Uncited references*: This section comprises references that occur in the reference list but not in the body of the text. Please position each reference in the text or delete it. Any reference not dealt with will be retained in this section.

Queries and/or remarks

Location in Article	Query/remark
Introduction section, fourth paragraph	Cocaign and Lindley (1993) was changed and linked to Cocaign et al. (1993). Please check if appropriate.
Introduction section, fourth paragraph	Cocaign-Bousquet et al. (1995) was changed and linked to Cocaign-Bousquet and Lindley (1995). Please check if appropriate.
Materials and methods section, stress induced by lactic acid subsection, first paragraph	The incomprehensible construction of the sentence "As stationary phase an organic acid resin (CS Chromatography, Langerwehe, Germany) and as eluent 1 mM H ₂ SO ₄ with a flow rate of 0.6 ml/min was used." was rephrased to "As stationary phase, an organic acid resin (CS Chromatography, Langerwehe, Germany) was used, while as eluent, it was a 1-mM H ₂ SO ₄ with a flow rate of 0.6 ml/min." Please check if appropriate.

Thank you for your assistance.

Fax to: (202) 315-5796; (703) 562-1873 and (703) 562-1913
(If you're faxing from the USA)
+1-(202) 315-5796; +1-(703) 562-1873 and +1-(703) 562-1913
(If you're faxing from other countries)



Re: Applied Microbiology and Biotechnology DOI 10.1007/s00253-006-0436-0
Metabolic activity of

Authors: Seletzky · Noack · Fricke · Hahn · Buchs

I. Permission to publish

Dear Raymond Leyva,

I have checked the proofs of my article and

- I have **no corrections**. The article is ready to be published without changes.
- I have **a few corrections**. I am enclosing the following pages:
- I have made **many corrections**. Enclosed is the **complete article**.

II. Offprint order

- Offprint order enclosed
- I do not wish to order offprints

Remarks:

Date / signature _____

III. Copyright Transfer Statement (sign only if not submitted previously)

The copyright to this article is transferred to Springer-Verlag (for U.S. government employees to the extent transferable) effective if and when the article is accepted for publication. The author warrants that his/her contribution is original and that he/she has full power to make this grant. The author signs for and accepts responsibility for releasing this material on behalf of any and all co-authors. The copyright transfer covers the exclusive right to reproduce and distribute the article, including reprints, translations, photographic reproductions, microform, electronic form (offline, online) or any other reproductions of similar nature.

An author may self-archive an author-created version of his/her article on his/her own website and his/her institution's repository, including his/her final version; however he/she may not use the publisher's PDF version which is posted on www.springerlink.com. Furthermore, the author may only post his/her version provided acknowledgement is given to the original source of publication and a link is inserted to the published article on Springer's website. The link must be accompanied by the following text: "The original publication is available at www.springerlink.com."

The author is requested to use the appropriate DOI for the article (go to the Linking Options in the article, then to OpenURL and use the link with the DOI). Articles disseminated via www.springerlink.com are indexed, abstracted and referenced by many abstracting and information services, bibliographic networks, subscription agencies, library networks, and consortia.

After submission of this agreement signed by the corresponding author, changes of authorship or in the order of the authors listed will not be accepted by Springer.

Date / Author's signature _____

Offprint Order Form

- To determine if your journal provides free offprints, please check the journal's instructions to authors.
- If you do not return this order form, we assume that you do not wish to order offprints.**
- If you order offprints **after** the issue has gone to press, costs are much higher. Therefore, we can supply offprints only in quantities of 300 or more after this time.
- For orders involving more than 500 copies, please ask the production editor for a quotation.

Please enter my order for:

Pages	1-4	1-4	5-8	5-8	9-12	9-12	13-16	13-16	17-20	17-20	21-24	21-24	25-28	25-28	29-32	29-32
Copies	EUR	USD	EUR	USD	EUR	USD	EUR	USD	EUR	USD	EUR	USD	EUR	USD	EUR	USD
<input type="checkbox"/> 50	250.00	275.00	300.00	330.00	370.00	405.00	430.00	475.00	500.00	550.00	525.00	575.00	575.00	630.00	610.00	670.00
<input type="checkbox"/> 100	300.00	330.00	365.00	405.00	465.00	510.00	525.00	580.00	625.00	685.00	655.00	720.00	715.00	785.00	765.00	840.00
<input type="checkbox"/> 200	400.00	440.00	525.00	575.00	645.00	710.00	740.00	815.00	860.00	945.00	925.00	1,015.00	1,005.00	1,105.00	1,105.00	1,190.00
<input type="checkbox"/> 300	500.00	550.00	680.00	750.00	825.00	910.00	955.00	1,050.00	1,095.00	1,205.00	1,190.00	1,310.00	1,295.00	1,425.00	1,425.00	1,530.00
<input type="checkbox"/> 400	610.00	670.00	855.00	940.00	1,025.00	1,130.00	1,195.00	1,315.00	1,360.00	1,495.00	1,485.00	1,635.00	1,615.00	1,775.00	1,775.00	1,915.00
<input type="checkbox"/> 500	720.00	790.00	1,025.00	1,130.00	1,225.00	1,350.00	1,430.00	1,575.00	1,625.00	1,780.00	1,780.00	1,960.00	1,930.00	2,125.00	2,090.00	2,300.00

Orders will only be processed if a credit card number has been provided. For German authors, payment by direct debit is also possible.

I wish to be charged in Euro USD

Prices include surface mail postage and handling.
 Customers in EU countries who are not registered for VAT should add VAT at the rate applicable in their country.

VAT registration number (EU countries only):

Please charge my credit card

- Eurocard/Access/Mastercard
 American Express
 Visa/Barclaycard/Americard

Number (incl. check digits):

Valid until: __ / __

Date / Signature: _____

For authors resident in Germany: payment by direct debit:

I authorize Springer to debit the amount owed from my bank account at the due time.

Account no.: _____

Bank code: _____

Bank: _____

Date / Signature: _____

Send receipt to:

- Jochen Buchs
 Biochemical Engineering, RWTH Aachen
 University, Sammelbau Biologie,
 Worringerweg 1, 52056, Aachen,
 Germany

Ship offprints to:

- Jochen Buchs
 Biochemical Engineering, RWTH Aachen
 University, Sammelbau Biologie,
 Worringerweg 1, 52056, Aachen,
 Germany

